

# EXTRAPOLATION/INTERPOLATION OF INFINITE DILUTION ACTIVITY COEFFICIENT DATA BETWEEN SOLVENTS

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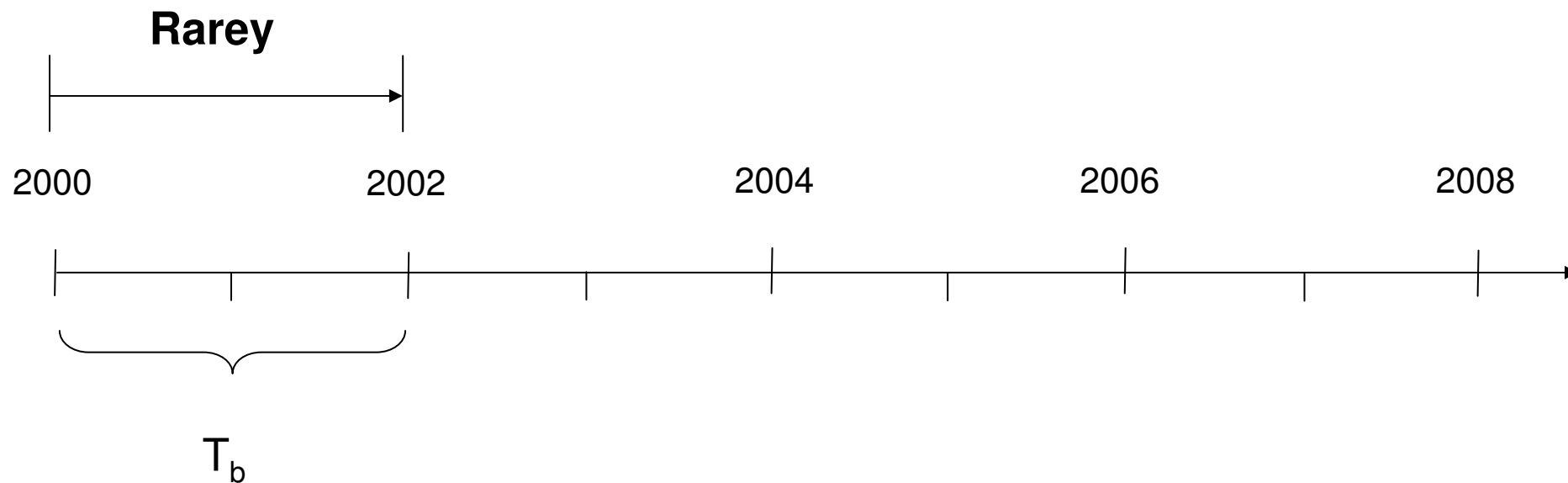
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## Overview

- Project Background
- Extrapolation in the Case of Alkane Solvents
- Applications
- Alcohol Interpolation between Alkanes and Water
- Further Work
- Acknowledgements

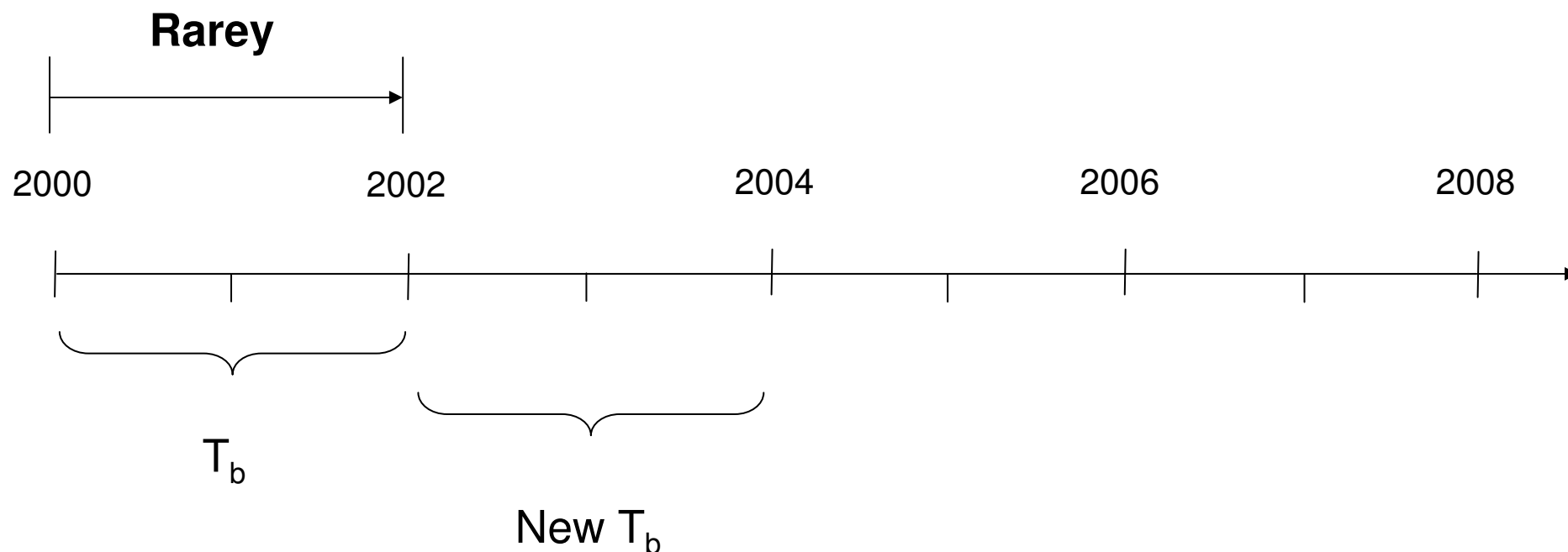


## Project Background



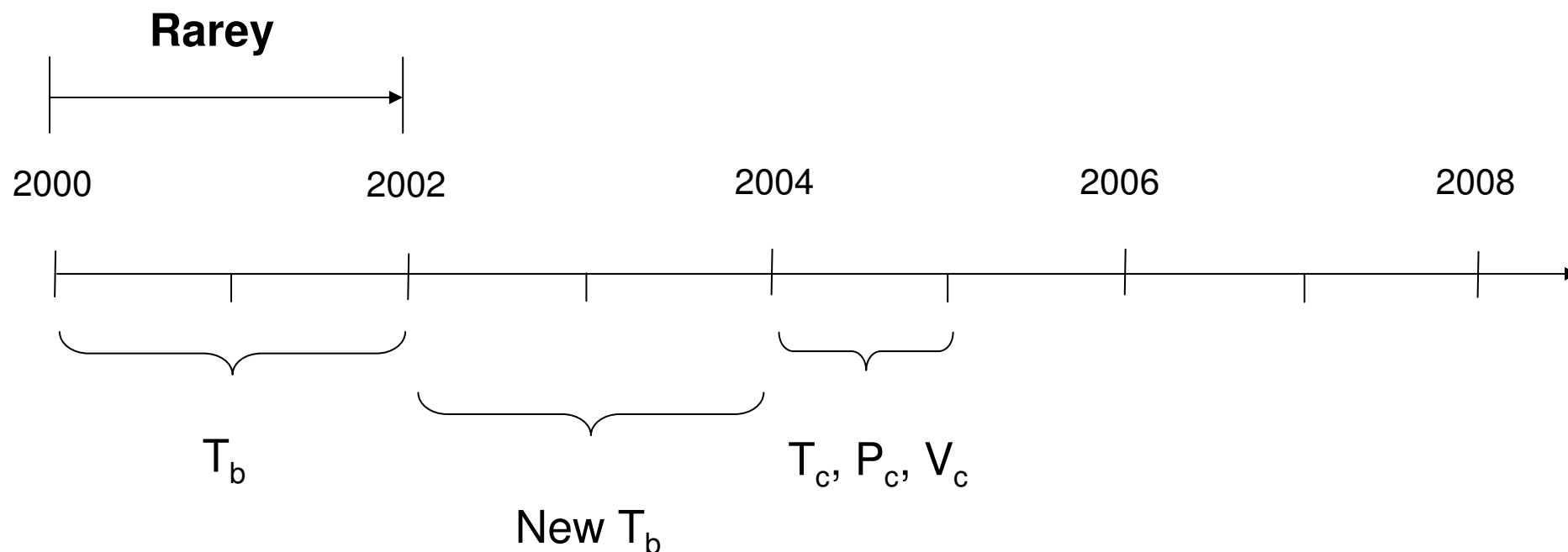
W. Cordes, J. Rarey, *A New Method for the Estimation of the **Normal Boiling Point** of Non-Electrolyte Organic Compounds*, Fluid Phase Equilibria, 201/2, 397-421 (2002).

## Project Background



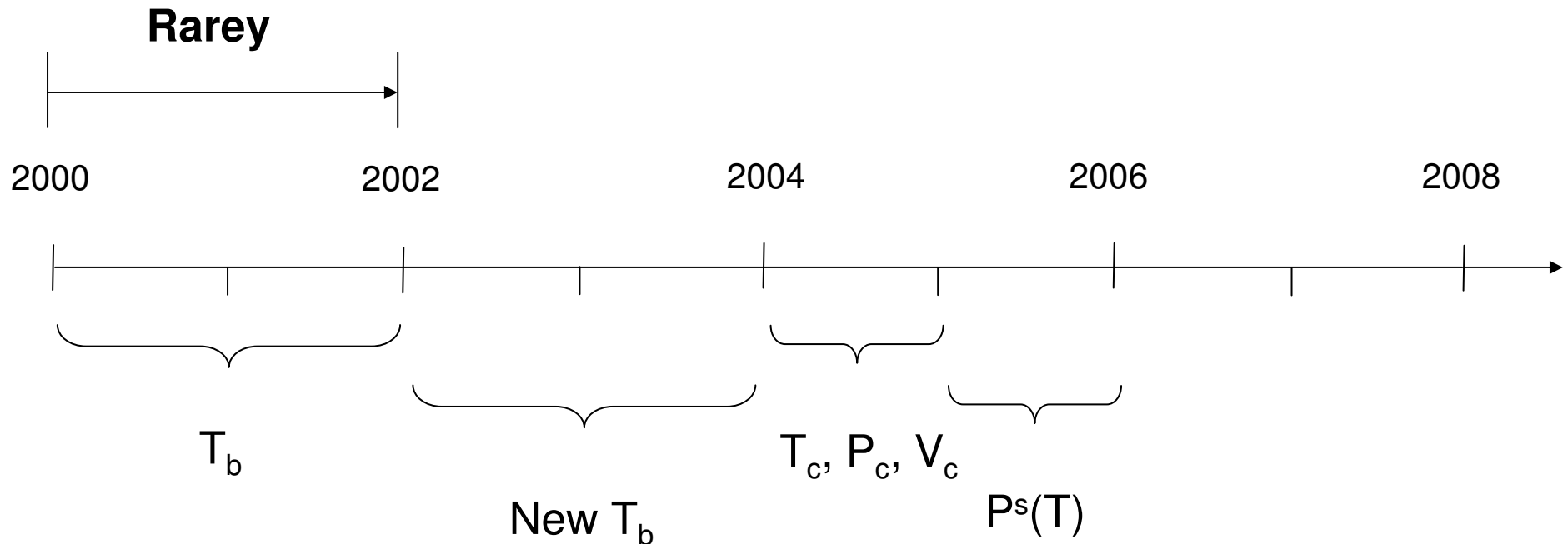
Y. Nannoolal, J. Rarey , D. Ramjugernath, W. Cordes, *Estimation of Pure Component Properties, Part 1: Estimation of the **Normal Boiling Point** of Non-Electrolyte Organic Compounds via Group Contributions and Group Interactions*, Fluid Phase Equilibria, 226, 45-63, 2005.

## Project Background



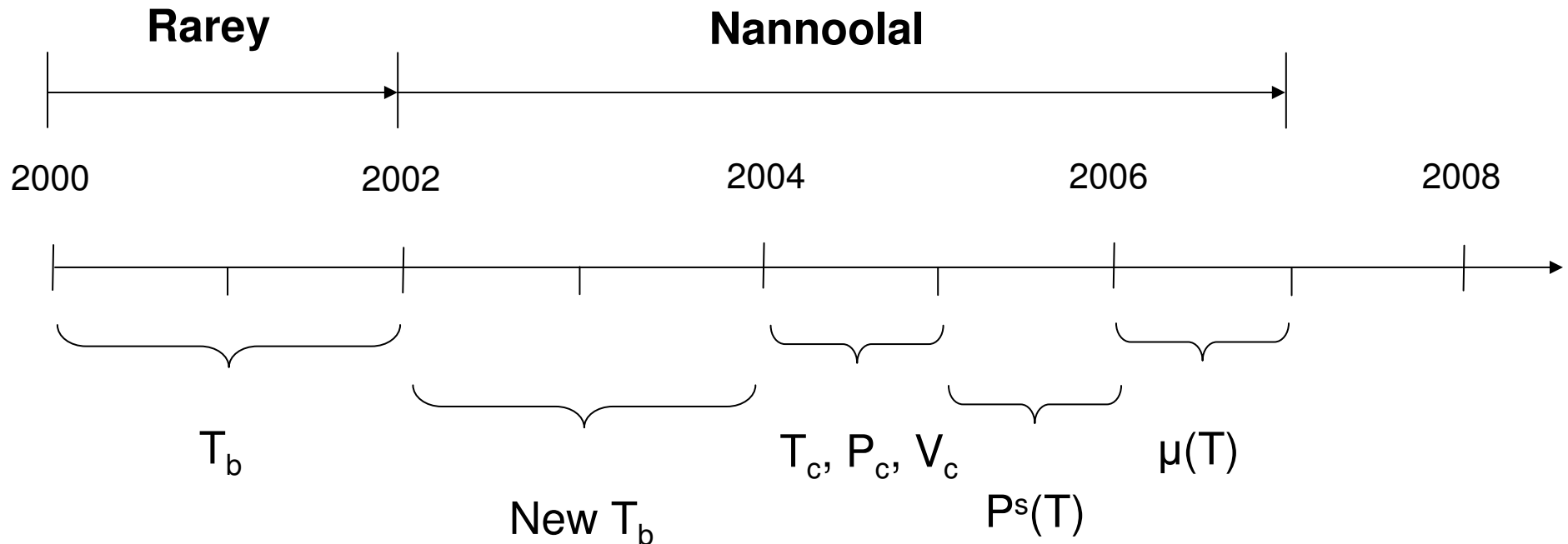
Nannoolal, Y., Rarey, J., Ramjugernath, D., Estimation of Pure Component Properties Part 2: Estimation of **Critical Data** by Group Contribution., *Fluid Phase Equilib.*, 252 (2007) 1.

## Project Background



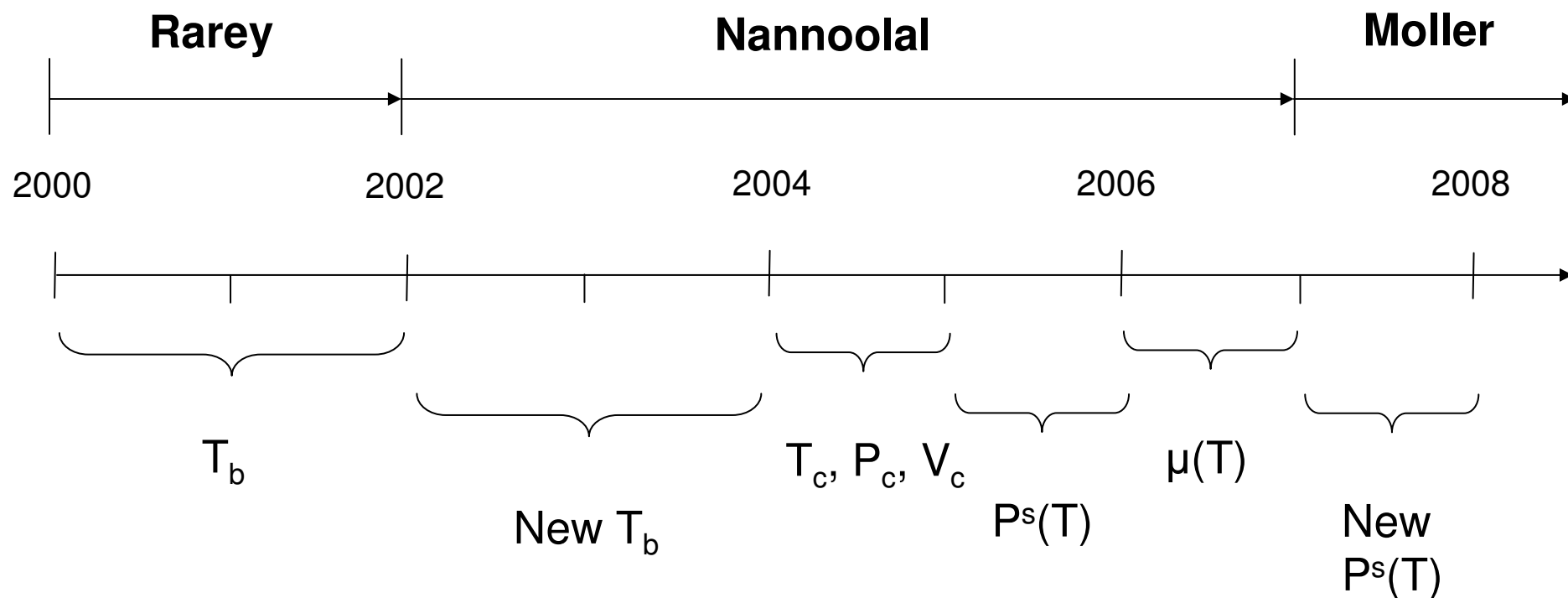
Nannoolal, Y., Rarey, J., Ramjugernath, D., Estimation of Pure Component Properties Part 3: Estimation of the **Vapour Pressure** of Non-Electrolyte Organic Compounds via Group Contributions and Group Interactions., *Fluid Phase Equilib.* 267 (2008) 117.

## Project Background



Nannoolal, Y., Rarey, J., Ramjugernath, D., Estimation of Pure Component Properties Part 4: Estimation of the **Liquid Viscosity** of Non-Electrolyte Organic Compounds via Group Contributions and Group Interactions., *Fluid Phase Equilib.* 281 (2009) 97

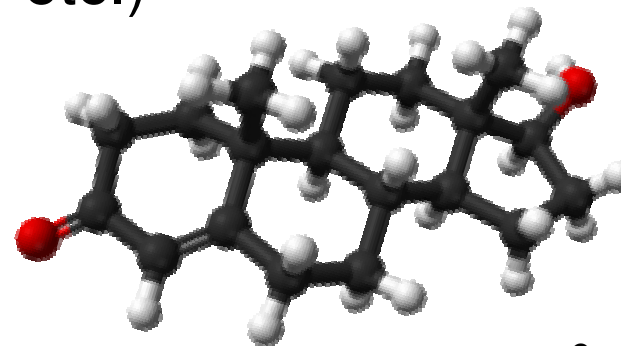
## Project Background



Moller, B., Rarey, J., Ramjugernath, D., Estimation of the **Vapour Pressure** of Non-Electrolyte Organic Compounds via Group Contributions and Group Interactions., *J. Mol. Liq.* 143 (2008) 52

## Project Background

- Current work:  
“Prediction of the activity of complex multifunctional organic compounds in common solvents”
- Useful for:
  - Design of separation equipment
  - Partitioning between compartments
  - ...
- Current methods (UNIFAC, COSMO etc.)



## Simplify the Problem

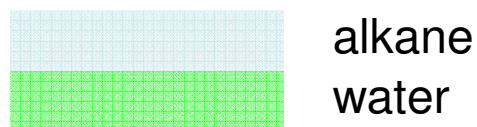
$$\gamma = f(x, T, P, \text{solvent}, \text{solute})$$

- Solvent
  - Only reference solvents
- Concentration
  - Solid solubility data mainly of interest
  - Only at infinite dilution ( $x < 0.01$ )
- Pressure
  - Small at low to moderate pressures
- Temperature
  - Non-trivial
  - Only at 298 K



## Available Data

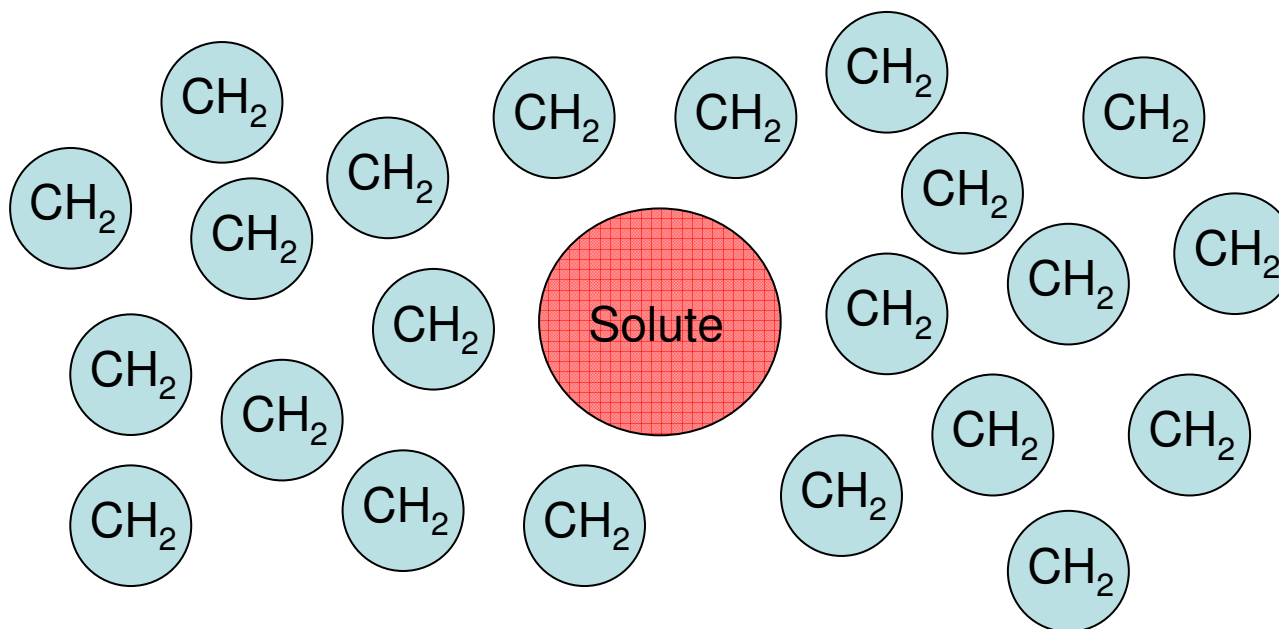
- Most frequent solvents in the Dortmund Data Bank ( $\gamma^\infty$  data)
  - Water
  - Others ???



Solvent	No. Solutes
Water	585
Squalane	207
Hexadecane	198
Sulfolane	137
1-Octanol	128
Phthalic acid dinonyl ester	126
Heptane	116
N-Methyl-2-pyrrolidone	115
Octadecane	103
19,24-Dioctadecyldotetracontane	99

## Reduction to a Common Solvent - Hexane

- Combinatorial and residual contribution
- Solution of groups concept:  
 “Residual contributions for a single solute in any alkane solvent **at infinite dilution** are identical”



## Reduction to a Common Solvent - Hexane

- Expressing this mathematically:
- Activity coefficient made up of a combinatorial and residual contribution:

$$\gamma_{1,hexane}^{\infty} = \gamma_{1,hexane}^{R,\infty} \times \gamma_{1,hexane}^{C,\infty}$$

$$\gamma_{1,squalane}^{\infty} = \gamma_{1,squalane}^{R,\infty} \times \gamma_{1,squalane}^{C,\infty}$$

## Reduction to a Common Solvent - Hexane

- Expressing this mathematically:
- Taking the ratio, the residuals cancel:

$$\frac{\gamma_{1,hexane}^{\infty}}{\gamma_{1,squalane}^{\infty}} = \frac{\cancel{\gamma_{1,hexane}^{R,\infty}} \times \gamma_{1,hexane}^{C,\infty}}{\cancel{\gamma_{1,squalane}^{R,\infty}} \times \gamma_{1,squalane}^{C,\infty}}$$

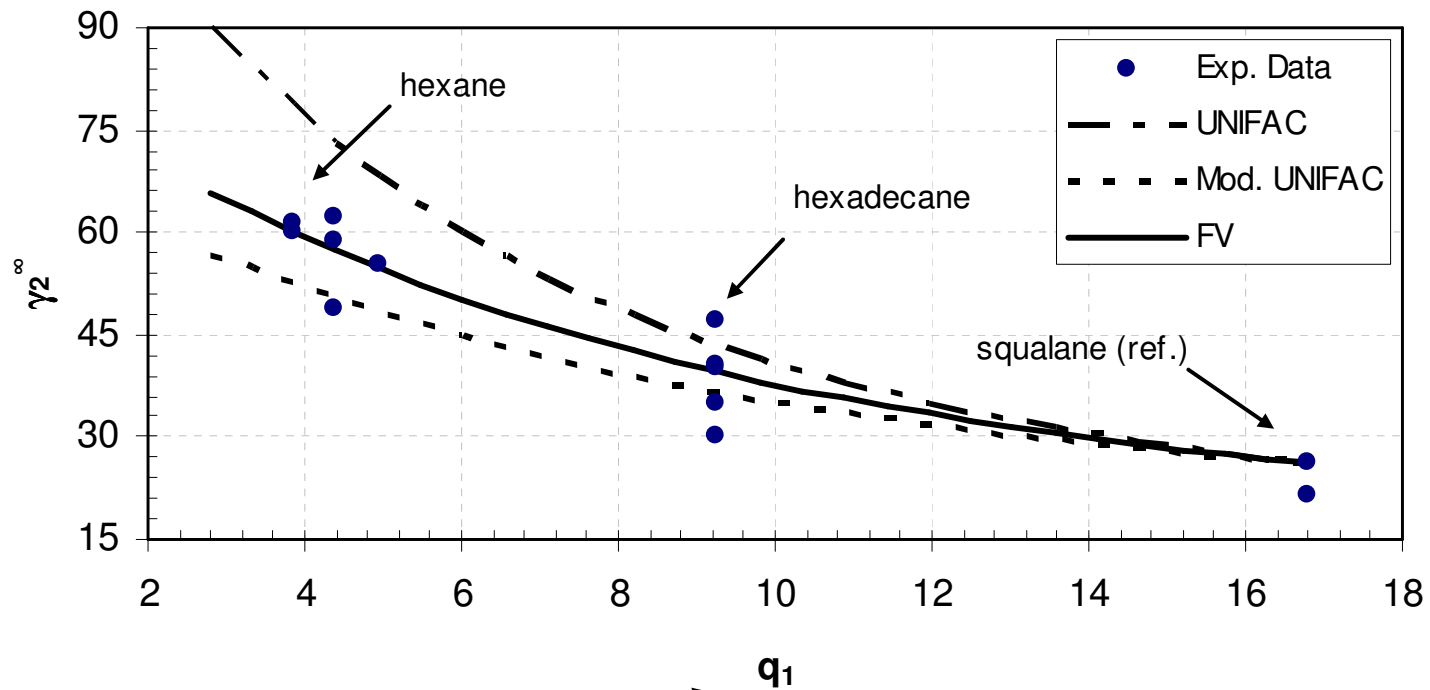
## Reduction to a Common Solvent - Hexane

- Expressing this mathematically:
- In general form:

$$\gamma_{1,hexane}^{\infty} = \gamma_{1,reference}^{\infty} \frac{\gamma_{1,hexane}^{C,\infty}}{\gamma_{1,reference}^{C,\infty}}$$

# Performance of Combinatorial Expressions

- Ethanol (2) in alkanes (1) ...

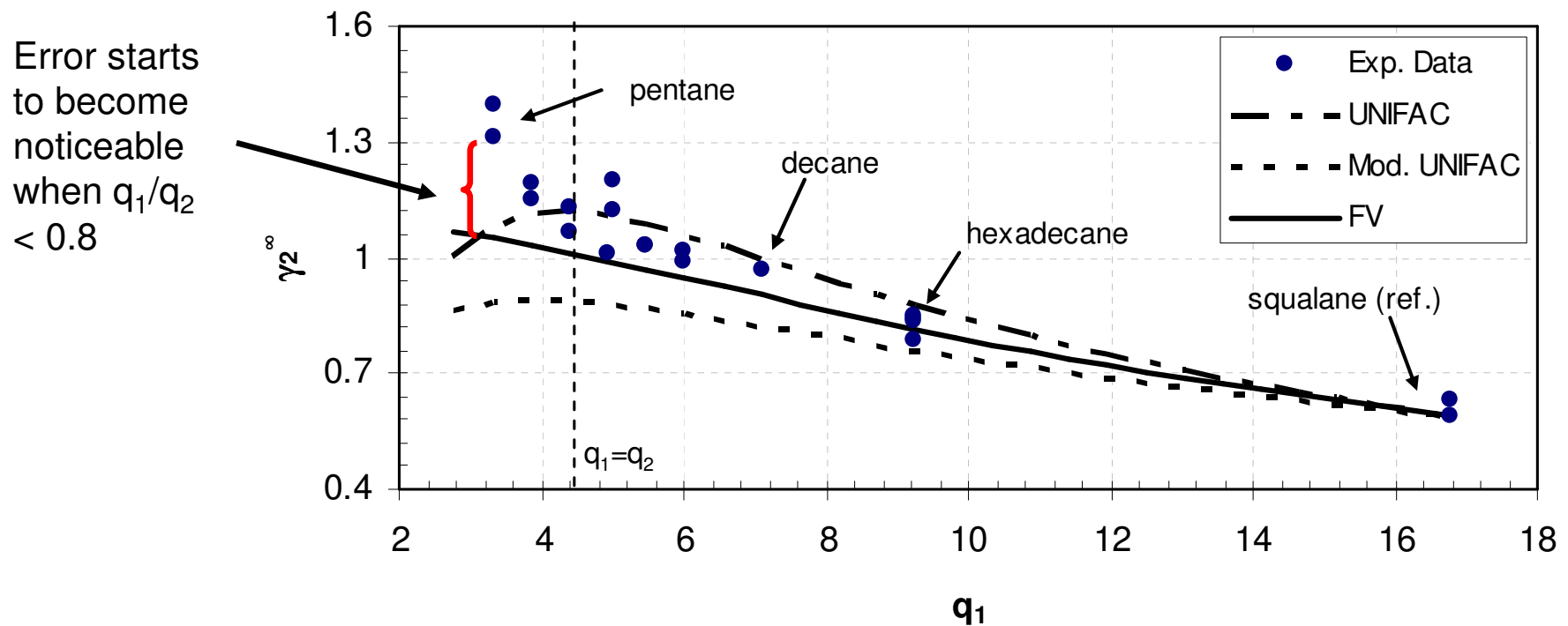


The UNIQUAC surface area for the alkane solvent

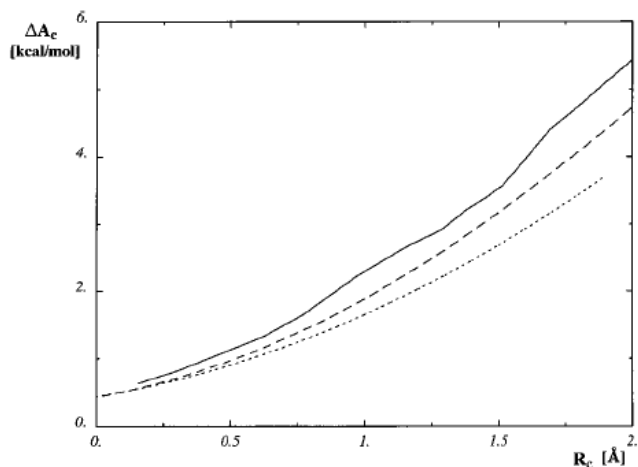
FV – Free Volume

## Performance of Combinatorial Expressions

- Ethylcyclohexane (2) in alkanes (1) ...

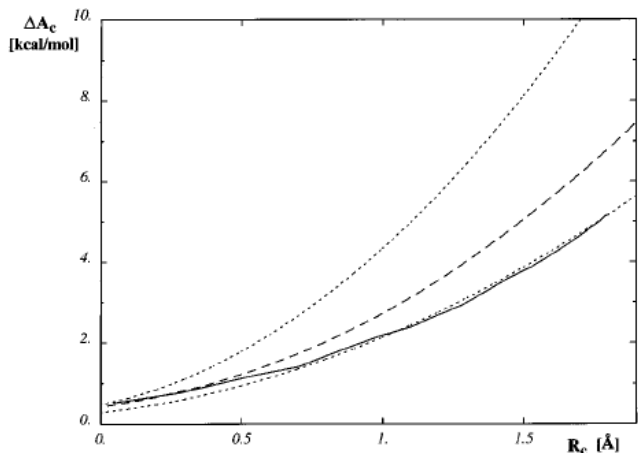


# Performance of Combinatorial Expressions



Work of cavity formation as a function of cavity size from molecular simulation [1] in:

**Hexane**



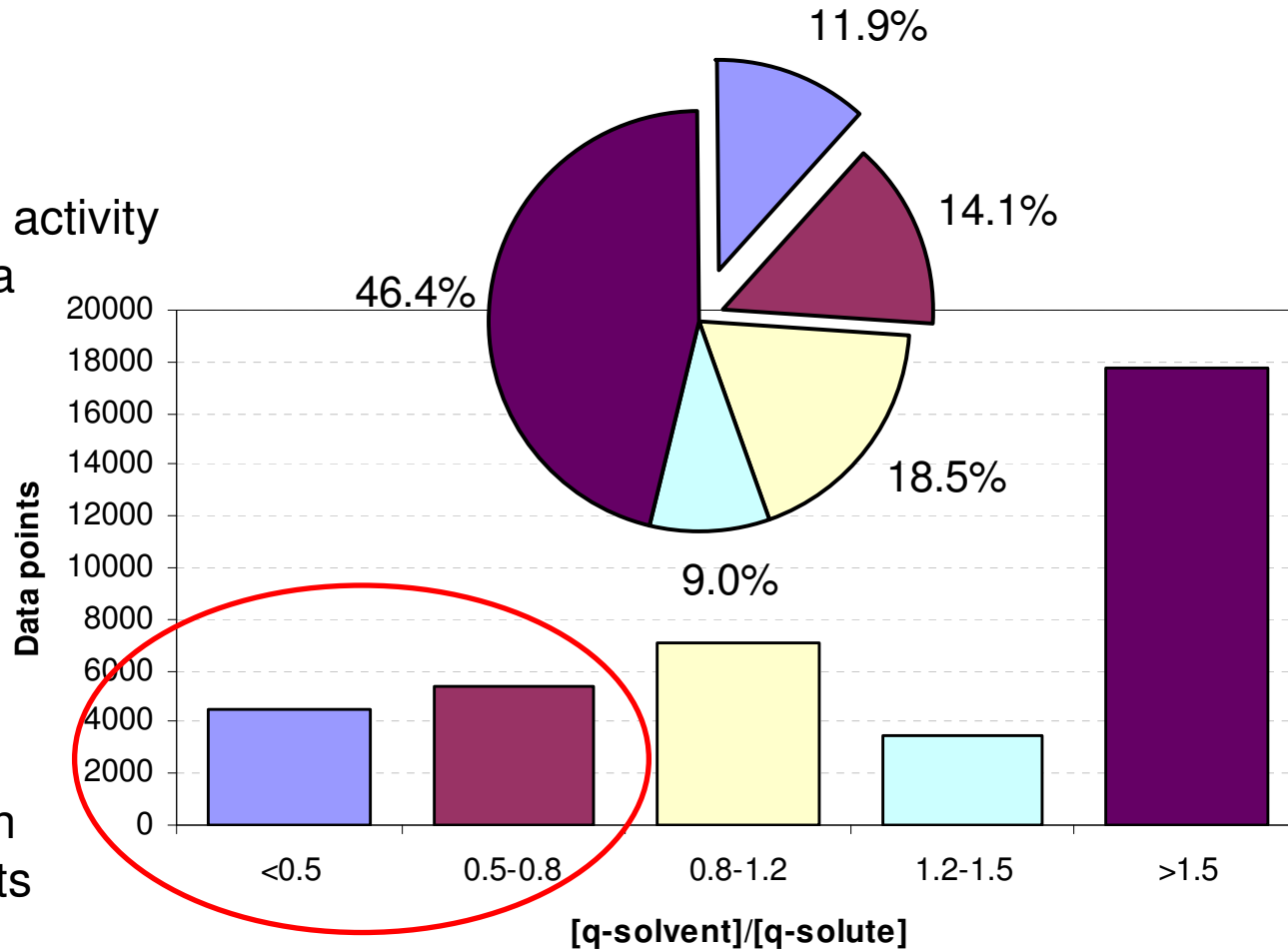
**Water**

Figure 2. Comparison of the work of cavity formation  $\Delta A_c$  computed with the two simulation methods RP (—) and TP (---) and with SP theory (- - -) as a function of the radius of the cavity  $R_c$  in hexane (a, top) and in water (b, bottom). In water, the upper and lower SP curves were computed with the  $\sigma$  (3.17 Å) and the most probable distance (2.8 Å), respectively.

[1] Prevost et al., Free Energy of Cavity Formation in Liquid Water and Hexane. *J. Phys. Chem.* **1996**, *100*, 2738-2743

# Performance of Combinatorial Expressions

Infinite dilution activity coefficient data



Big solutes in small solvents

## New Combinatorial Expression

- Propose the following correction to the combinatorial:

$$\ln \gamma_2^{\text{C-Cav},\infty} = \ln \gamma_2^{\text{C},\infty} + \ln \gamma_2^{\text{Cav},\infty}$$

Free-Volume Expression



$$\ln \gamma_2^{\text{Cav},\infty} = \left( \frac{V_2^{\text{FV}}}{V_1^{\text{FV}}} - \frac{V_2^{\prime\text{FV}}}{V_1^{\prime\text{FV}}} \right)$$

$$V_i^{\prime\text{FV}} = (V_{m,i})^{2/3} - (V_i^*)^{2/3}$$

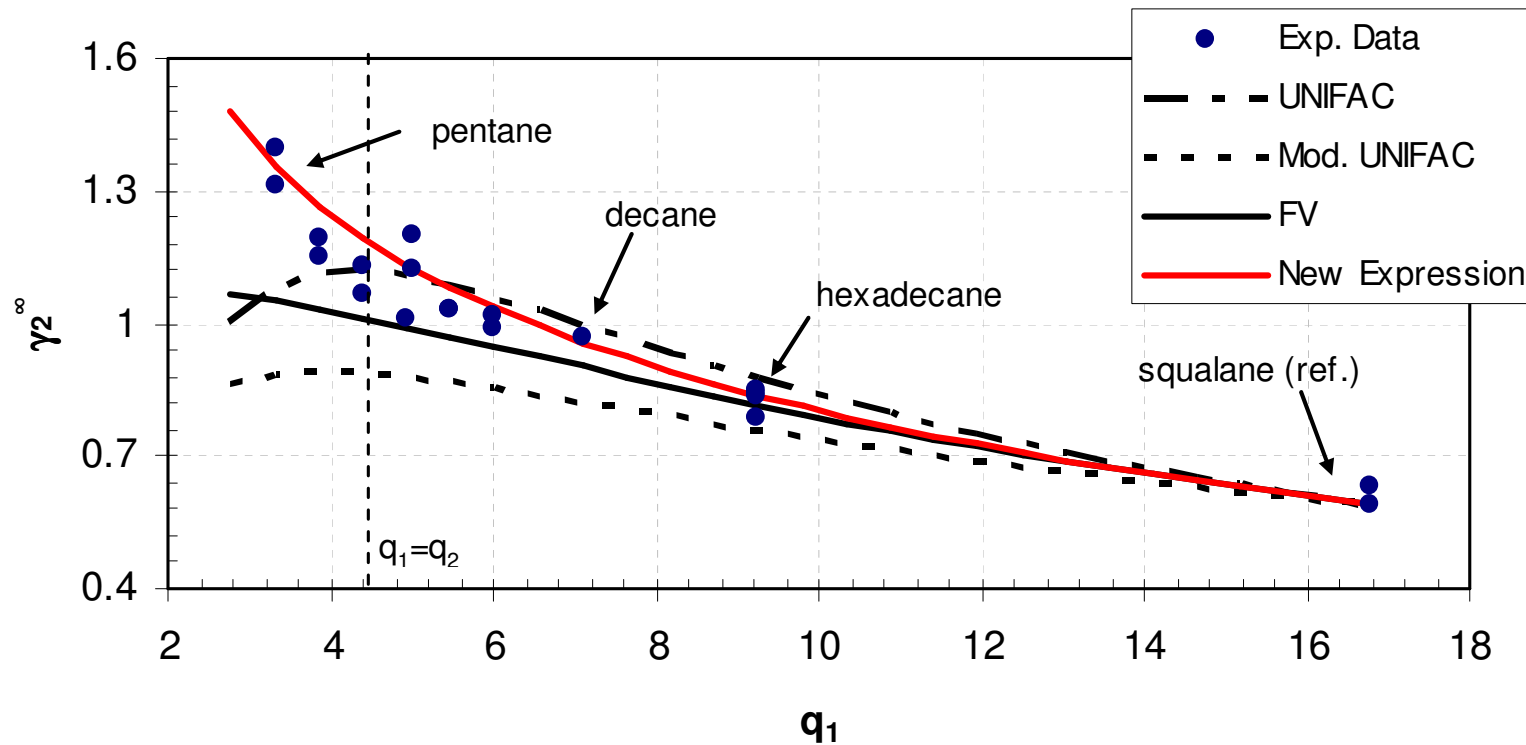
$V_{m,i}$  - Liquid molar volume (cm<sup>3</sup>/mol)

$$V_i^{\text{FV}} = V_{m,i} - V_i^*$$

$V_i^*$  - Van der Waals volume (cm<sup>3</sup>/mol)

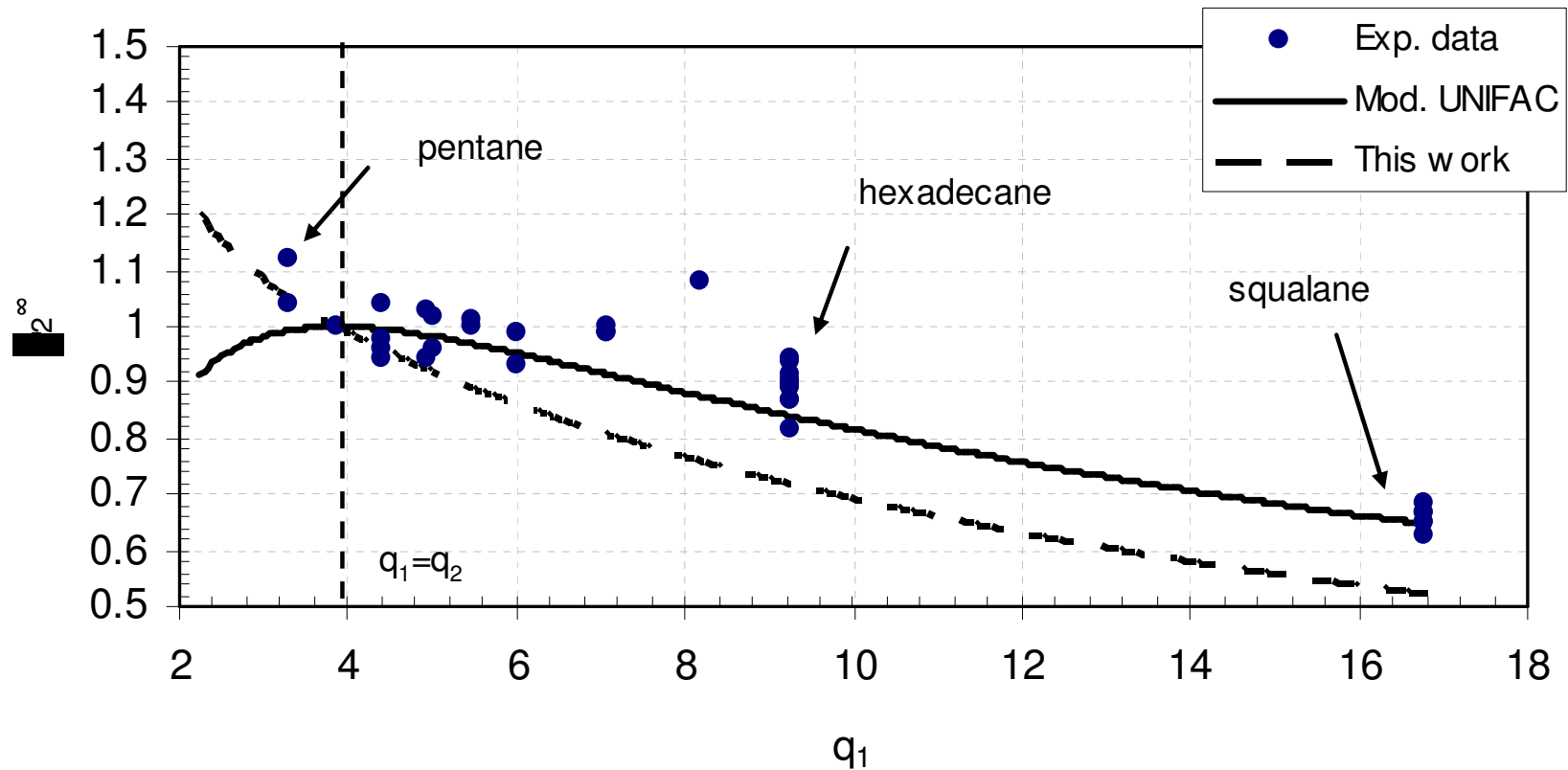
## Performance of the New Combinatorial Expression

- Ethylcyclohexane (2) in alkanes (1) ...



## Performance of the New Combinatorial Expression

- Hexane (2) in alkanes (1) ...



## Performance of the New Combinatorial Expression

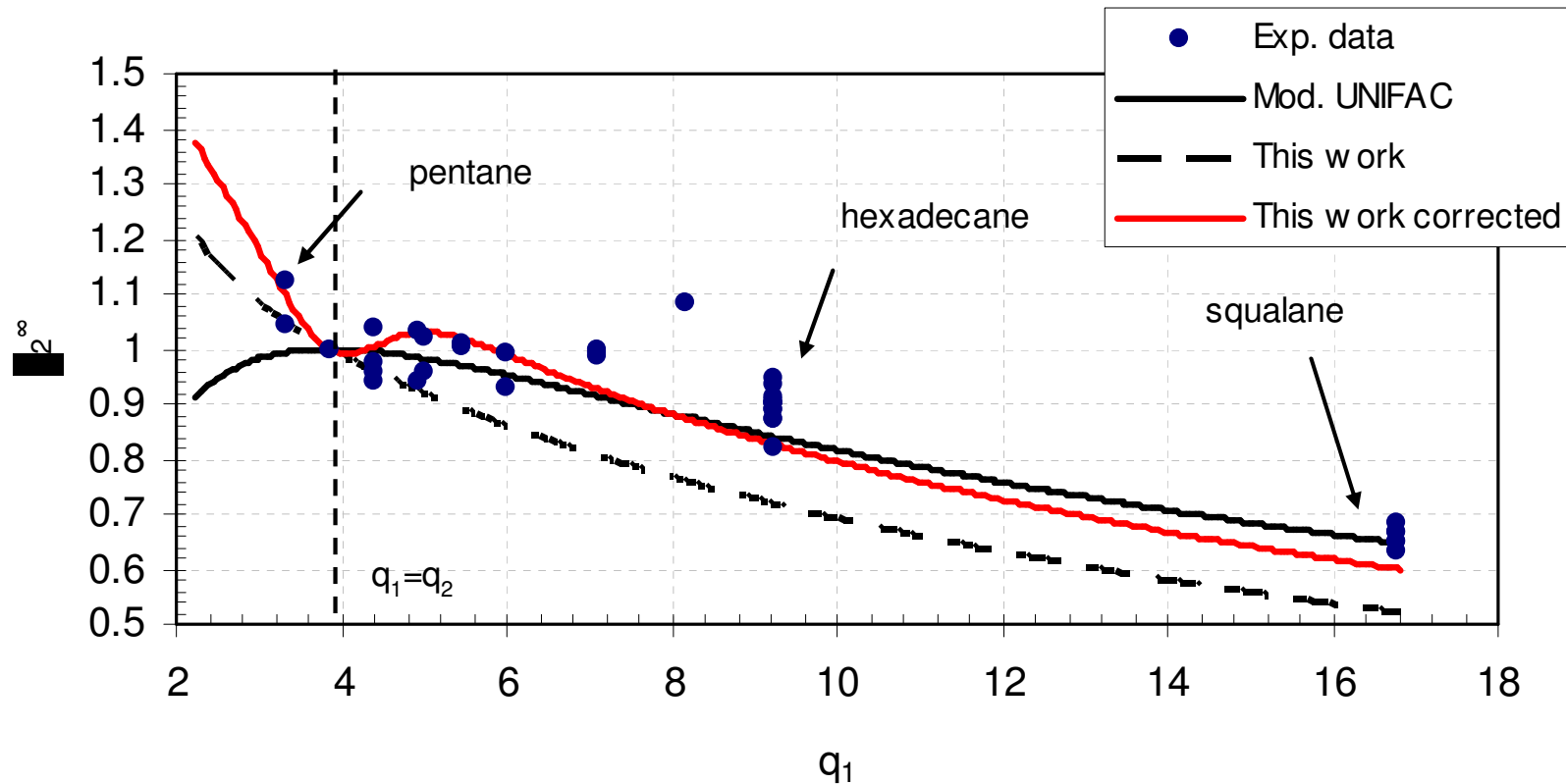
- Cavitation term empirically modified:

$$\gamma_2^{Cav,\infty} \Big|_{corrected} = \gamma_2^{Cav,\infty} \times \left( 1.15 - 0.15 \times \exp \left( -0.5(q_1 - q_2)^2 - 0.5(r_1 - r_2)^2 \right) \right)$$

- Step function allows an activity coefficient of 1 for pure component  $\gamma^\infty$

# Performance of the New Combinatorial Expression

- Hexane (2) in alkanes (1) ...



## Performance of the New Combinatorial Expression

‘Blindly’ (no changing of the parameters, only swapping the combinatorial expressions) applying this combinatorial expression to original UNIFAC:

Combinatorial	Relative Mean Deviation (%) in $\ln\gamma^\infty$	Number of data points
Original	88.0	29344
This work	71.1	29336

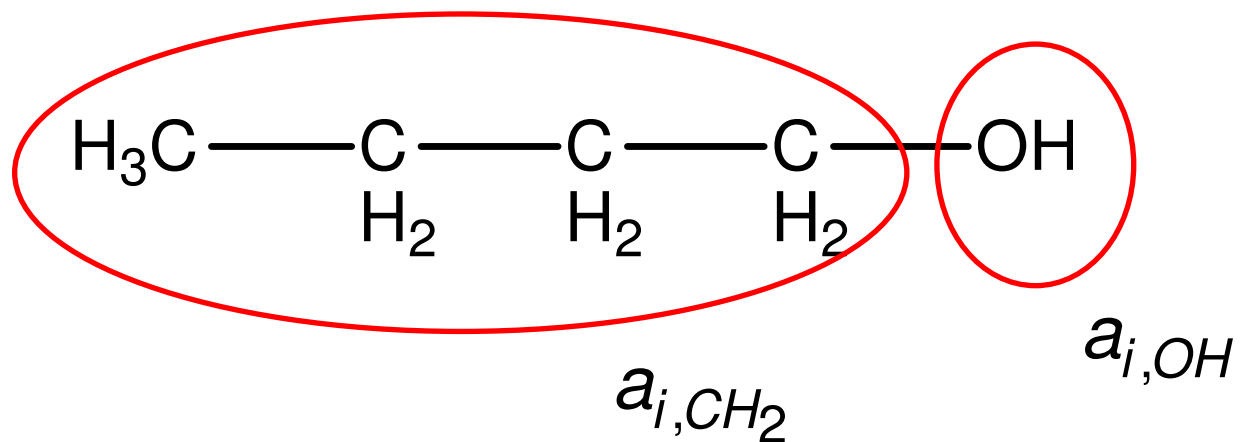
Note: Only data for water were excluded due to the combinatorial expression in this work giving unrealistically large values.

## Applications

- Development of combinatorial expressions
- Measurements of high boilers in low(er) boilers are difficult ...

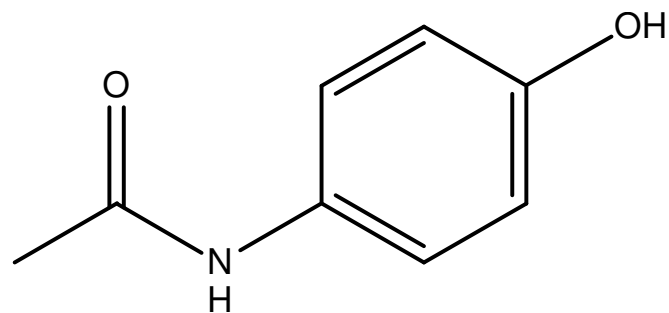


## Extension to Other Solvents - Alcohols



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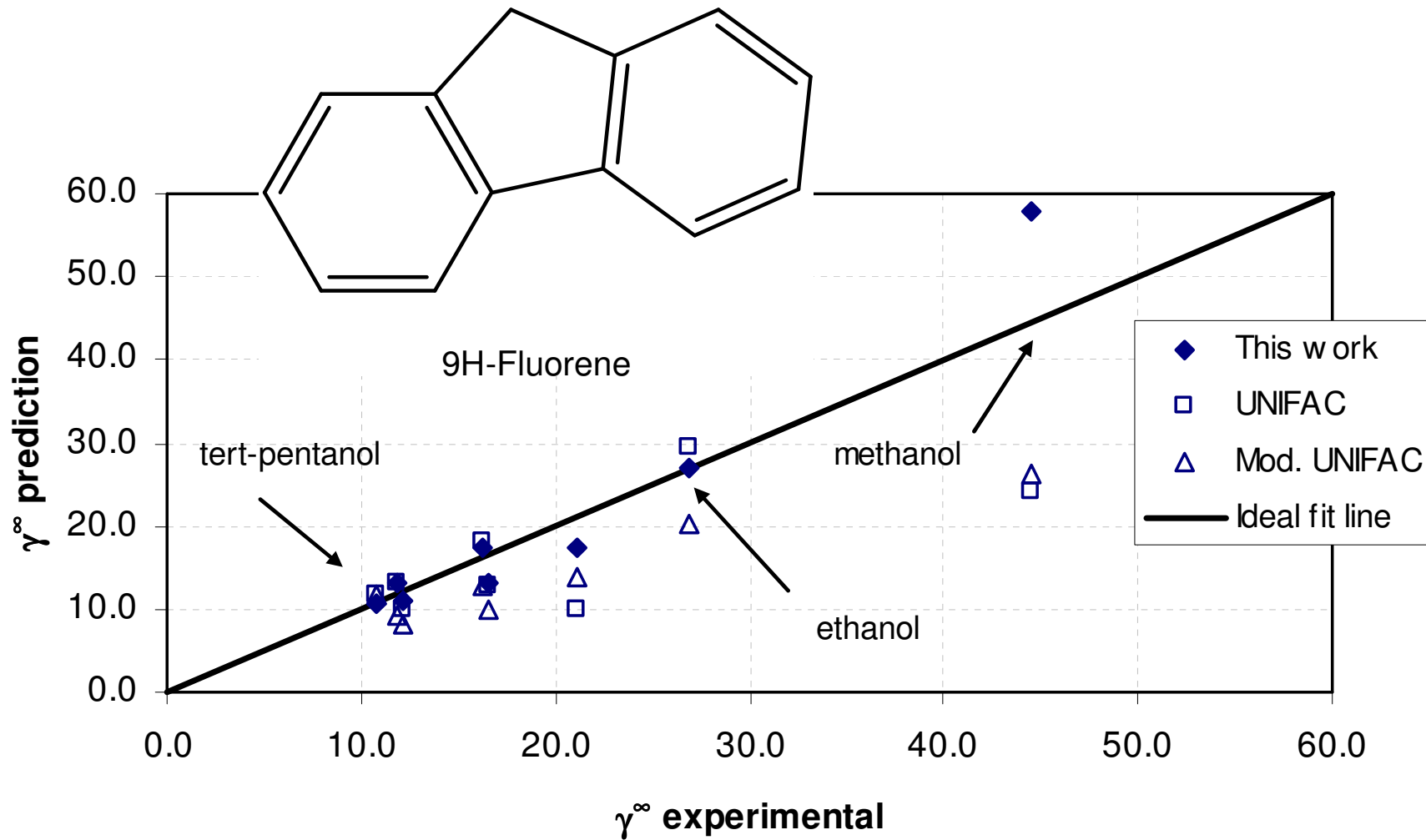
Solute



Paracetamol

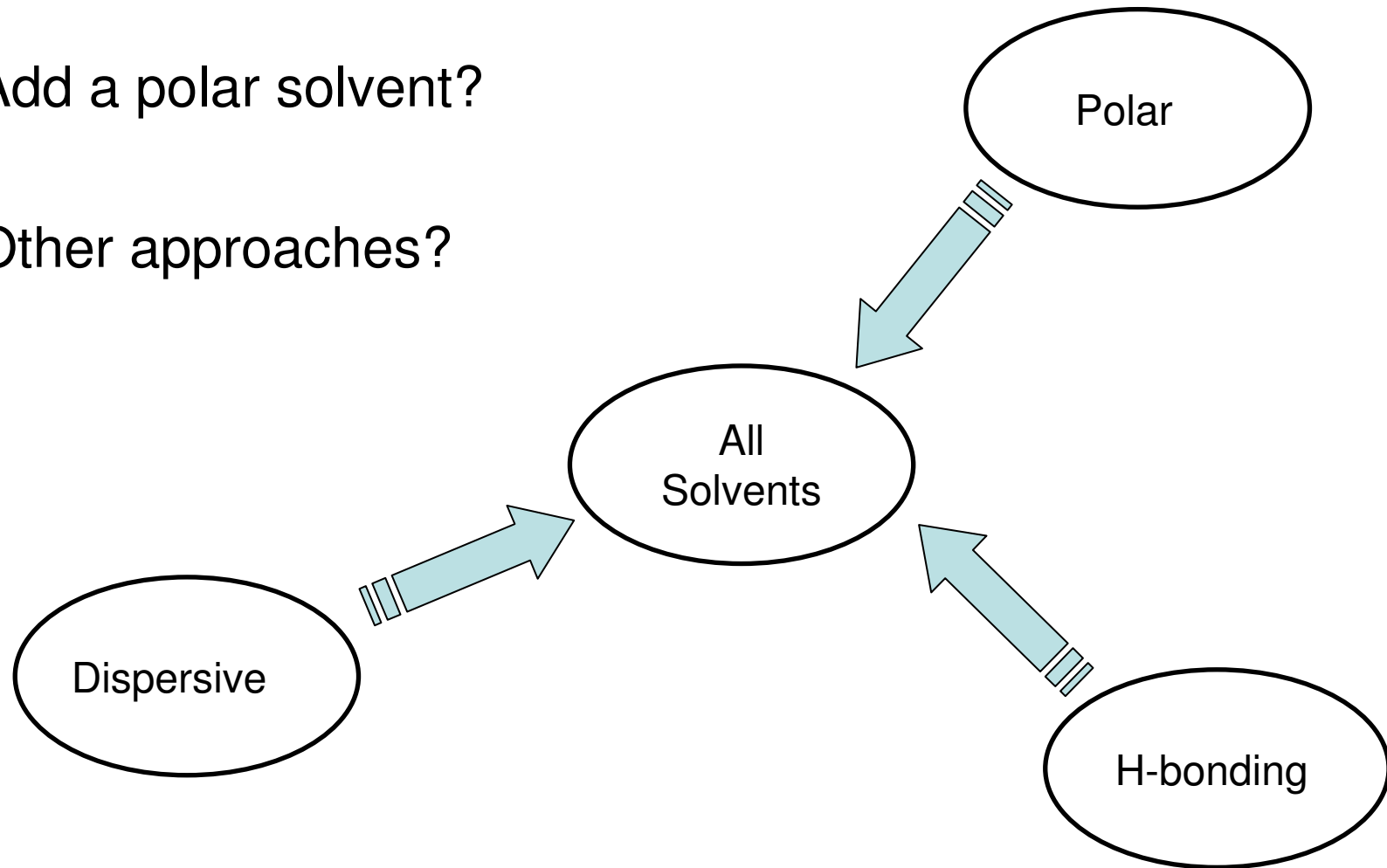
Solvent	$a_{OH}$	$a_{CH_3}$	$\gamma^\infty$ exp.	$\gamma^\infty$ pred.
Water	1.7	0		13
Ethanol	0.296	0.704	16.53	13.1
Hexane	0	2.2		764

# Extension to Other Solvents - Alcohols



## Further Work

- Add a polar solvent?
- Other approaches?



## Acknowledgements

- Supervisor:
  - Prof. J. Rarey
- Project Leaders:
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